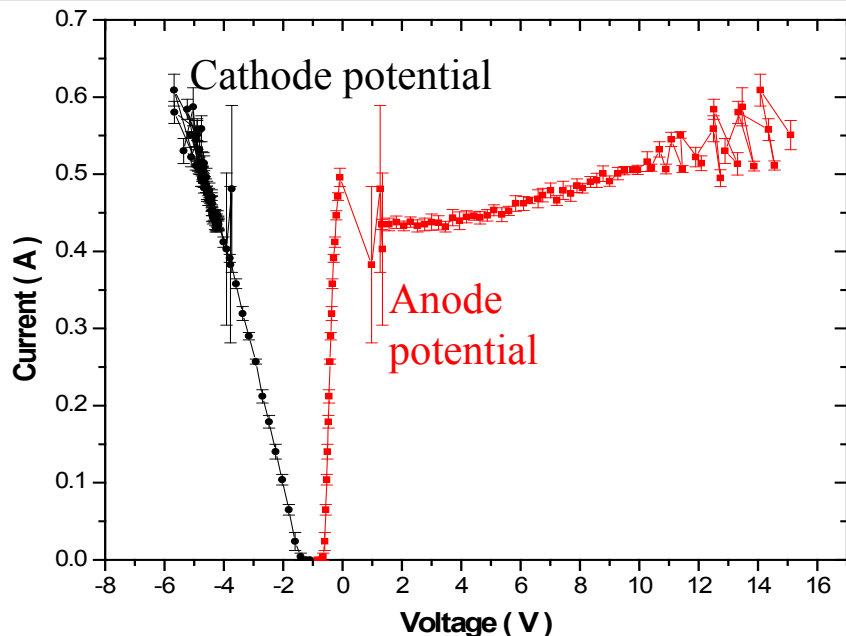


Quantitative EP Studies and Results for SRF Nb Cavity Production

Hui Tian

- **Basic understanding about Nb electropolishing helps to optimize the cavity EP process.**
- **Understanding the scale specific details of surface finishing after EP yield confident process control and optimization.**
- **Recent implications for Nb cavity production achieve promising results.**
- **Future work.**

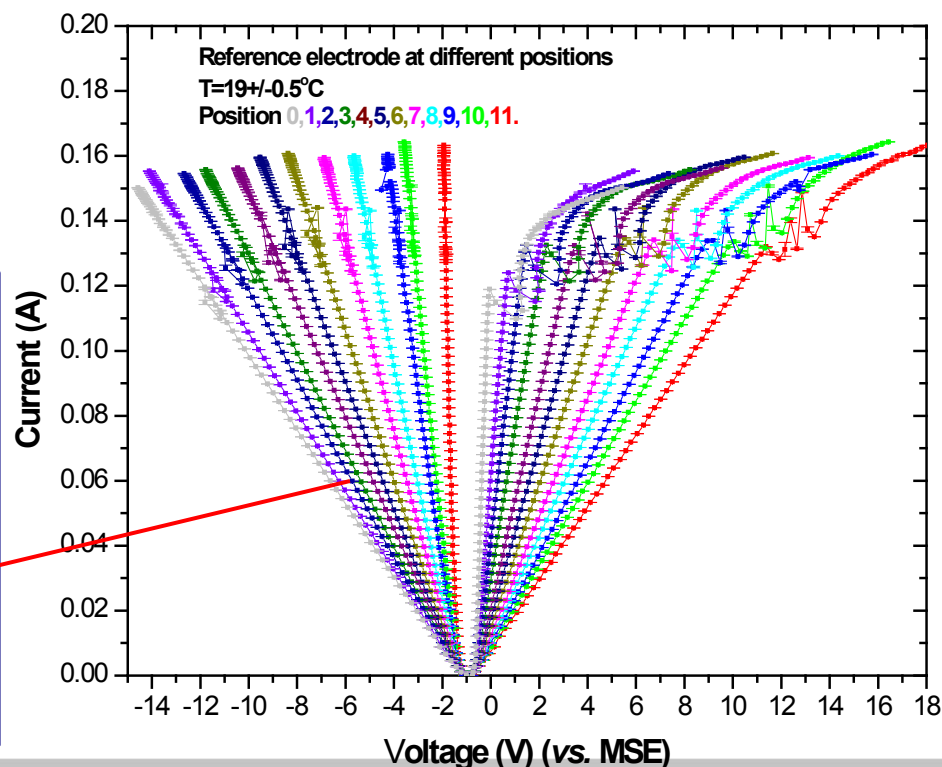
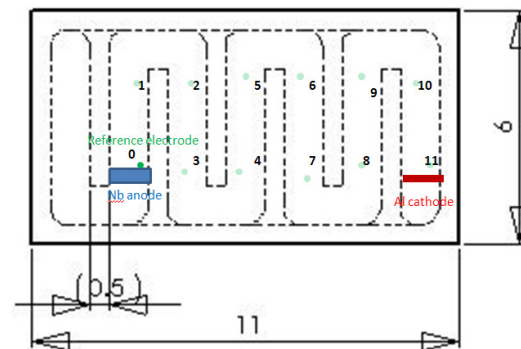
Understanding Potentials in Electrochemical Cell of Niobium EP



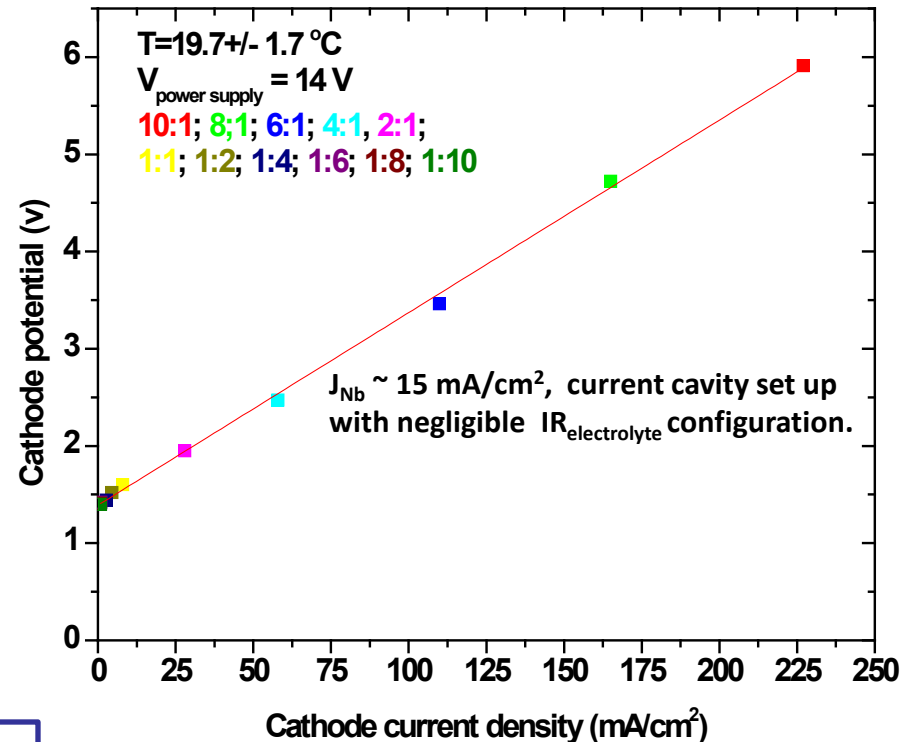
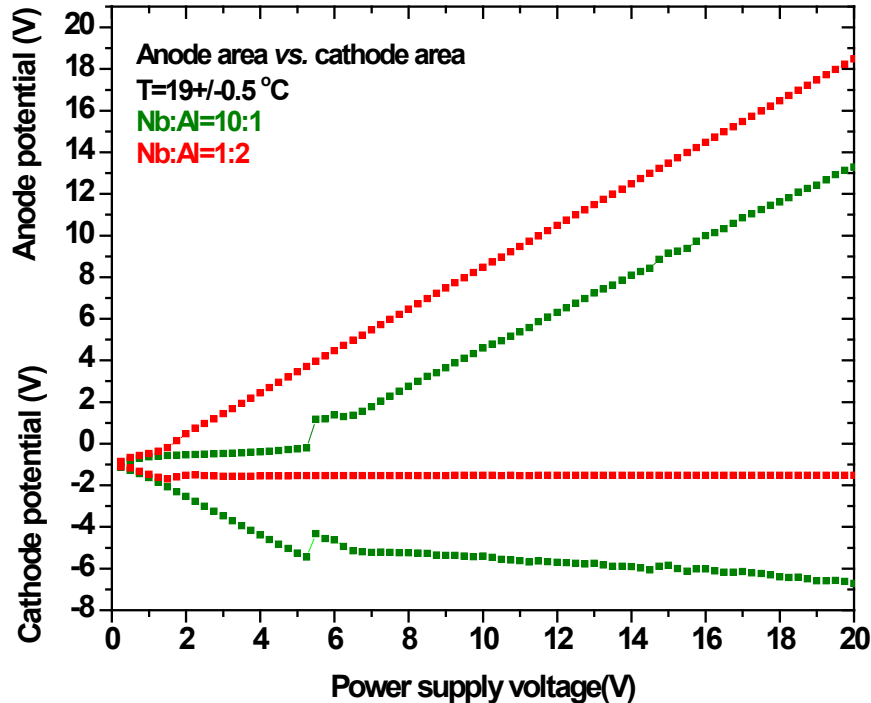
$$V_{\text{pwsup}} = (V_{\text{anode}} - V_{\text{cathode}}) + IR_{\text{electrolyte}} + IR_{\text{conduct}}$$

Monitoring I - V_{pwsup} only is inadequate to characterize the local EP effect on Nb.

Separate impacts of individual components in the Nb EP system: V_{anode} , V_{cathode} and $R_{\text{electrolyte}}$ (ρ @ 20 C ~ 13 ohm.cm)- those values depend on electrolyte composition, temperature, surface areas of cathode and anode, and geometry.



Large Cathode Surface Area Helps Decrease Cathode Potential

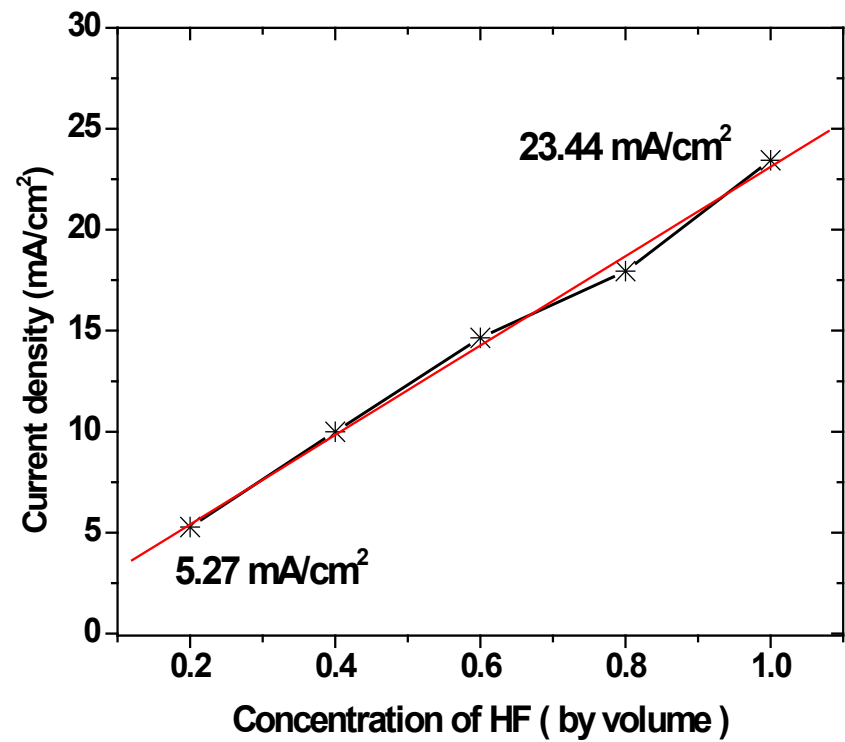
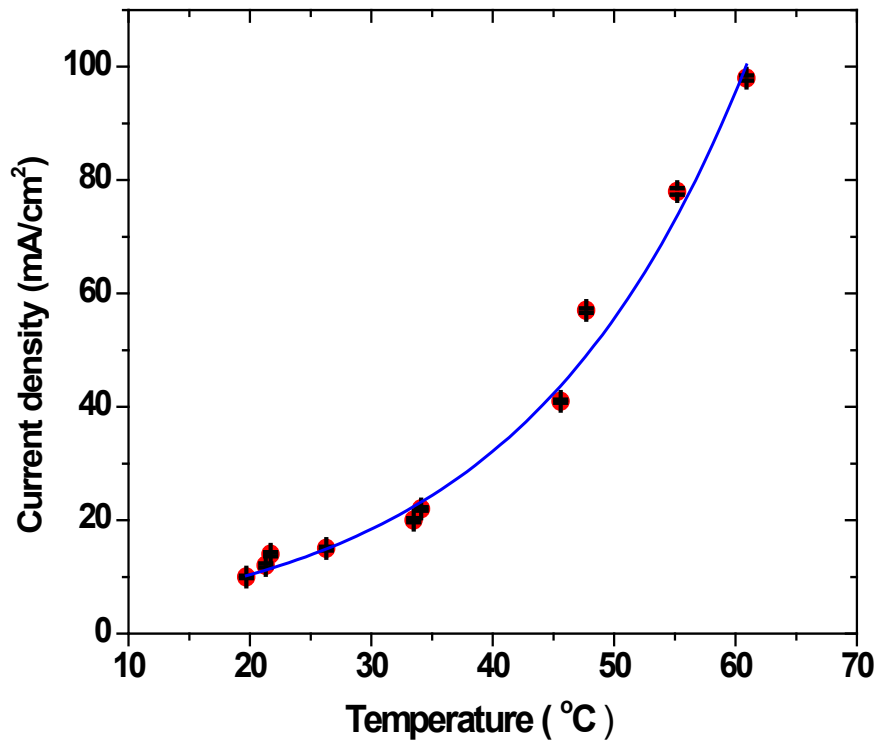


Beside extra power consumption due to low cathode area, high current density on the cathode and high over potential increases sulfur precipitation at the cathode.

"Sulfur Residues in Niobium Electropolishing", TUP0024, L. Zhao, H. Tian, C. Reece & M. Kelley.

Maximize cathode surface area or use new cathode material for improving hydrolysis at the cathode (less potential drop)

Anode Current Density Strongly Depends on Local Electrolyte Temperature & HF Concentration



The Nb anode plateau current density is directly proportional to the bulk F concentration, increases with temperature, and is independent of the amount of dissolved Nb.

Courtesy of 1) F. Eozénou et al. CARE-report-2008-022-SRF, 2) H. Tian, C. Reece, et al. J. Electrochem. Soc. 155(2008), p. D563

Current –Limited Plateau Is The Result of Mass-transfer Limitation

Mass transfer might occur by three mechanisms in an electrochemical cell. It is described by the Nernst-Planck equation, written for one-dimensional mass transfer along the x-axis as

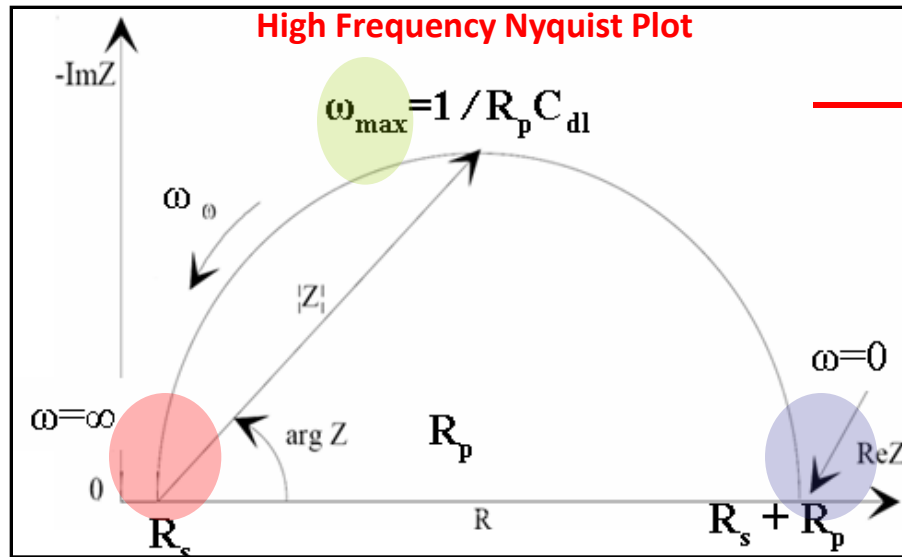
$$J_i(x) = -D_i \frac{\partial C_i(x)}{\partial x} - \frac{z_i F}{RT} D_i C_i \frac{\partial \phi(x)}{\partial x} + C_i v(x)$$

Diffusion, movement of mass transfer limited species by a concentration gradient

Migration, movement of ions driven by a gradient of electrical potential (for Nb Electropolishing, it is negligible in the plateau region)

Convection, natural convection driven by density gradient and forced convection, such as stirring, vibration, or pumped circulation

Use Electrochemical Impedance Spectroscopy (EIS) to Determine the Mechanism of Nb Electropolishing



$$Z = \frac{R_p}{1 + \omega^2 C_{dl}^2 R_p^2} + R_s - j \frac{\omega C_{dl} R_p^2}{1 + \omega^2 C_{dl}^2 R_p^2}$$

R_s : electrolyte, temperature.

R_p : temperature, concentration of reaction products, potential. (such as : salt film thickness etc),

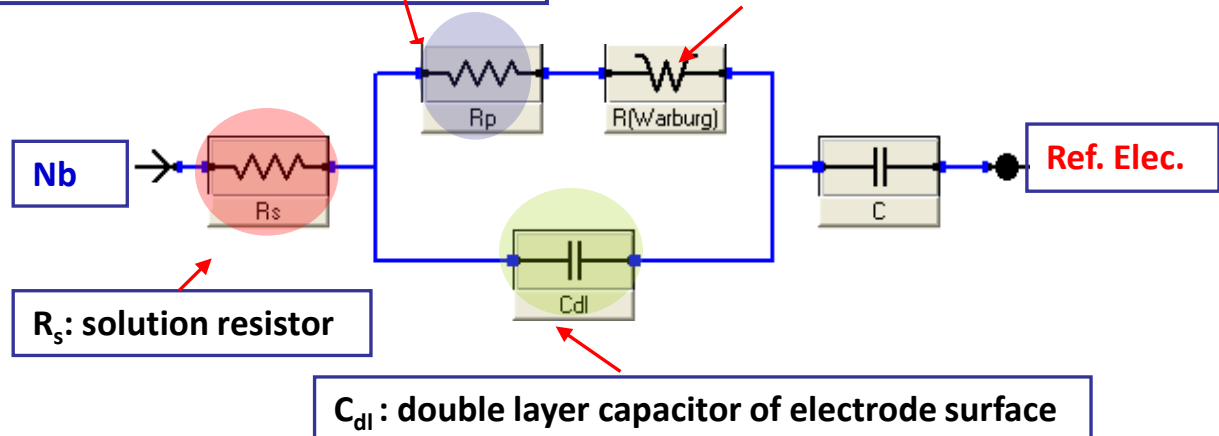
C_{dl} : electrolyte, temperature, potential, oxide layer, electrode roughness

R_w : the frequency of potential perturbation

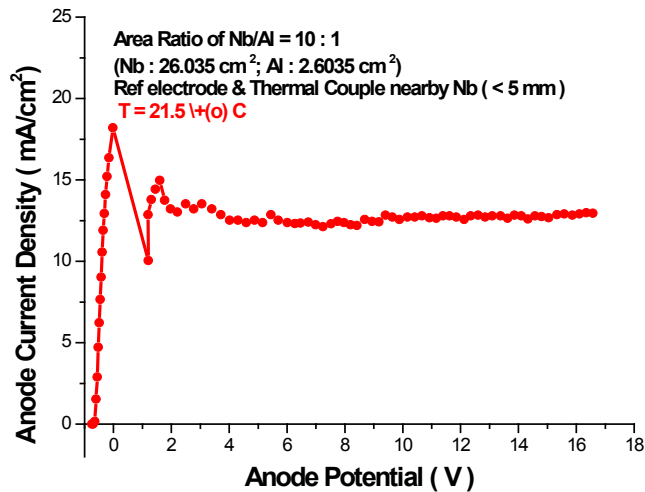
R_p : polarization/charger transfer resistor

R_{warburg} : diffusion resistor

Possible equivalent circuit of Nb-acid interface during Nb EP



EIS Study Discloses the Mechanism of Nb Electropolishing



T = 5.5 C, along the plateau region @ different potential, No agitation
HF : H₂SO₄ = 1 : 9

$$1.01 \text{ KHz} = \omega_{\max} = 1/R_p C_{dl}$$

$-Z_{\text{imag}}(\Omega)$

200 KHz

2V

3V

4V

5V

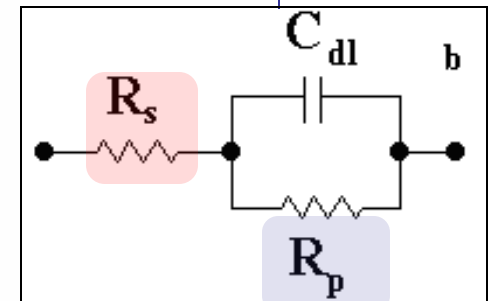
6V

7.8 V

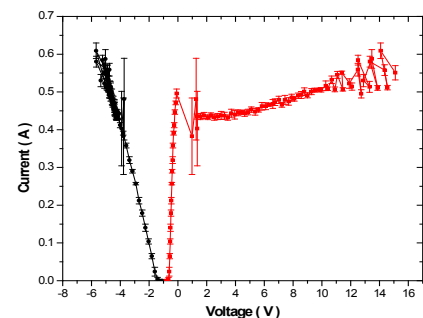
R_s remains constant

$Z_{\text{real}}(\Omega)$

R_p increases with the potential



The Diffusion-Limited Access of F^- to the Surface Produces Best Polishing

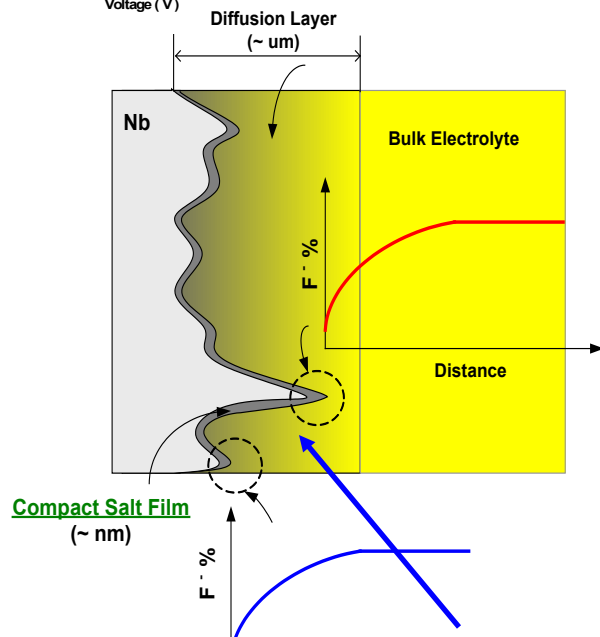


Anodization of Nb in H_2SO_4 produces Nb_2O_5 , but F^- aggressively dissolves Nb_2O_5 . These competing processes result in current flow and material removal.

Above a certain anodization potential (establishment of a salt film- Nb_2O_5), the reaction rate is limited by how fast F^- ions can arrive at the surface: diffusion limited mass transfer control.

The thickness of the salt film (Nb_2O_5) increases with applied potential (R_p), although the steady-state current does not change: current limited plateau.

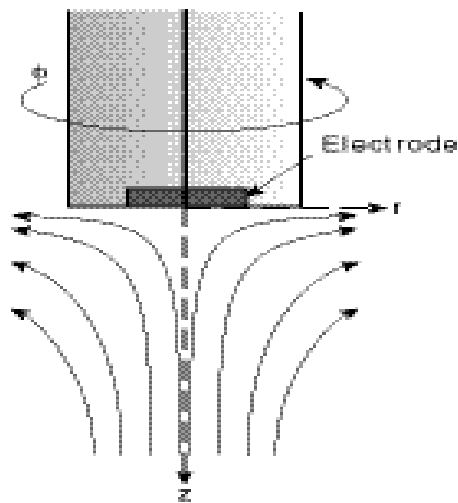
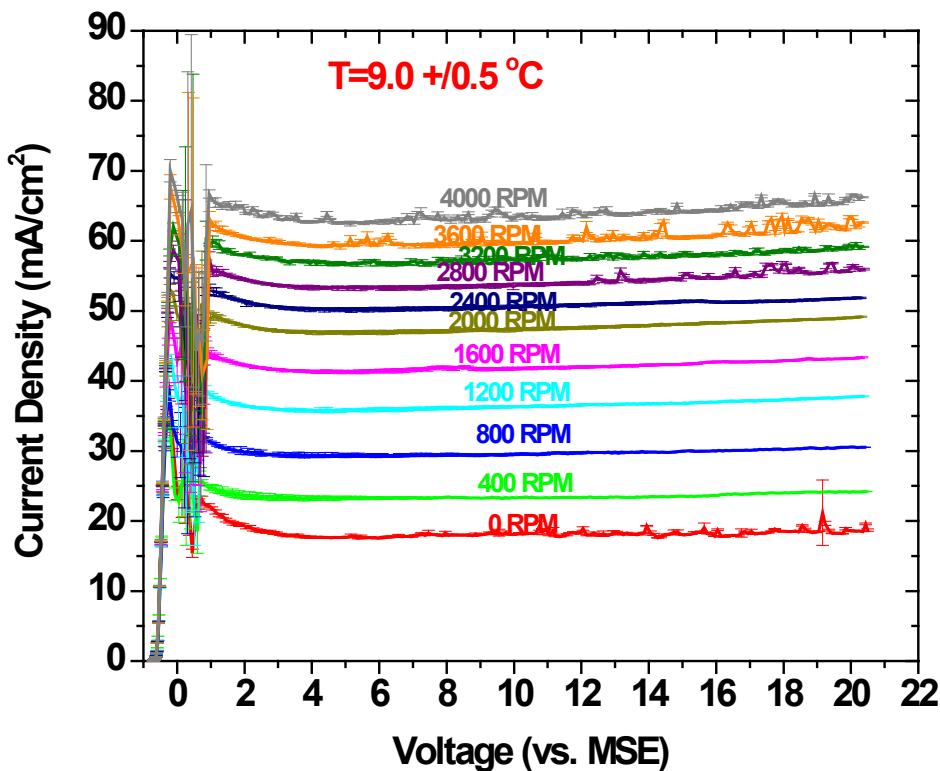
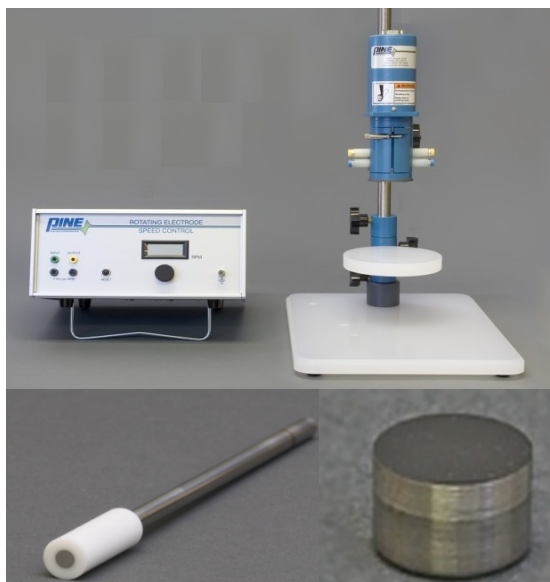
In the diffusion limited mass transfer only circumstance, diffusion is essentially isotropic and independent of the crystallographic orientation and grain boundary of the niobium surface: brightening.



Local temperature, flow (stirring, circulation) & electrolyte composition affect the local F^- gradient.

H. Tian, S. G. Corcoran, C. E. Reece and M. J. Kelley, *J. Electrochem. Soc.* 155(2008), p. D563.

Determination of the Diffusion Coefficient of Rate Limiting Species by Rotating Disk Electrode (RDE)



$$J = 0.62nFD^{0.67} \nu^{-0.166} c\omega^{0.5}$$

Levich equation

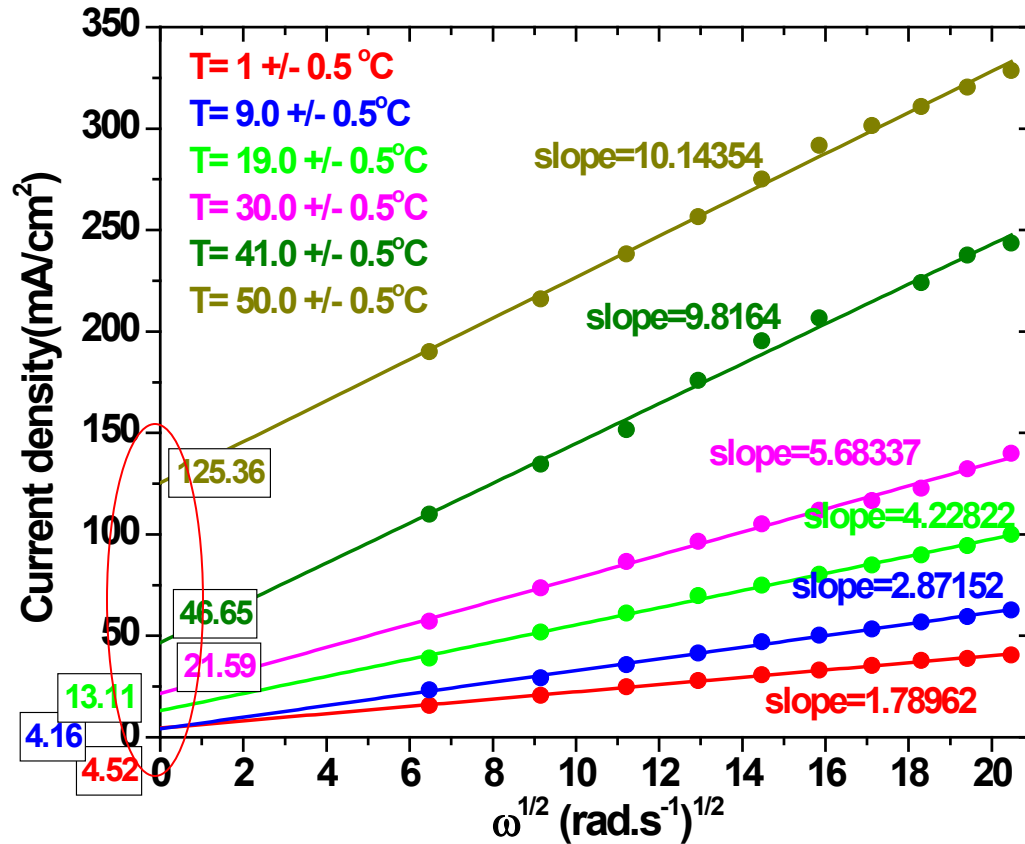
D : diffusion constant for diffusion limited species

ν : kinematic viscosity

ω : rotation speed of the electrode

c : bulk concentration of diffusion – limited species

RDE Measurements Indicate a Non-diffusion-limited Kinetics in Parallel and Strongly Depend on the Temperature



$$\text{slope}(J \text{ vs. } \omega^{0.5}) = 0.62nFD^{0.67} \nu^{-0.166} c$$

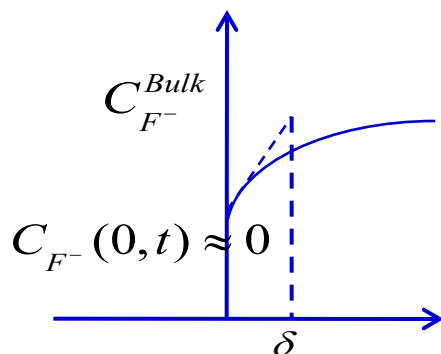
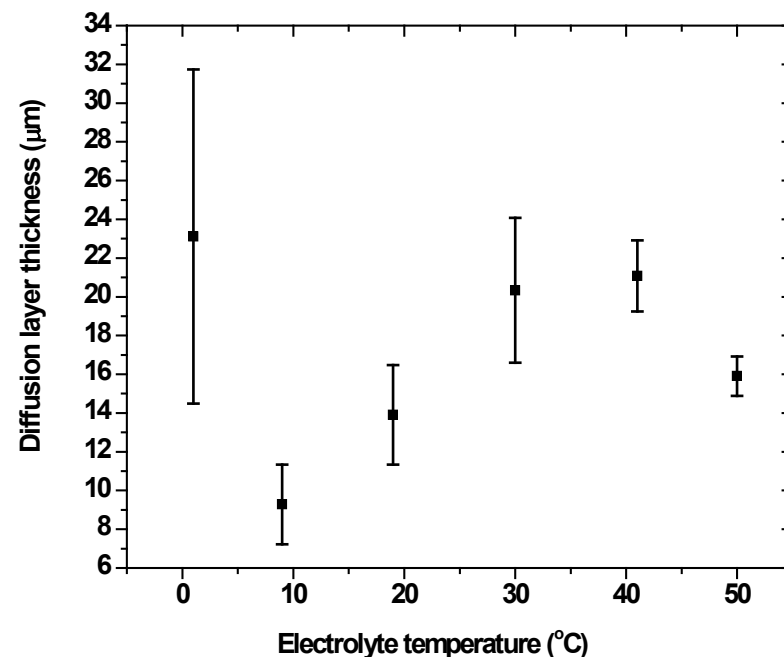
Excellent linear fit provides definitive evidence of diffusion limited process, knowing ν and c yields D .

H. Tian and C. E. Reece, PhysRev-STAB 13, 083502 (2010).

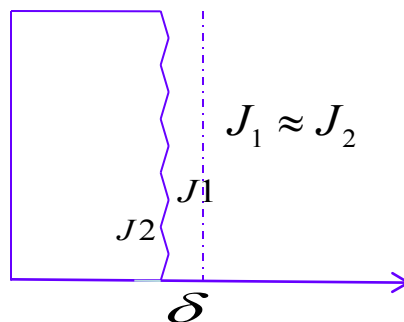
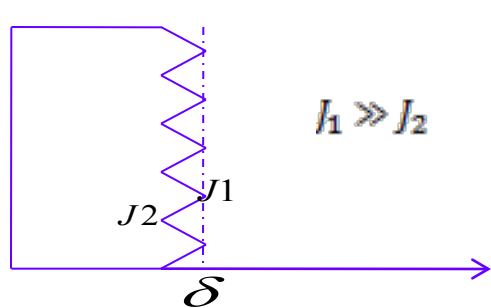
Strong evidence for a temperature dependent kinetics in parallel with the diffusion limited mass transfer process. For best polishing, stay below 20°C.

Electrolyte Physical Property and Diffusion Layer Thickness at Different Temperatures

Temperature (C)	Dynamic Viscosity (cP)	Diffusion Coefficient(cm ² /sec)
0	40.7	2.7E-08
10	34.2	4.4E-08
20	26.3	8.8E-08
30	20.8	1.3E-07
40	18.1	2.8E-07
50	16.5	2.9E-07



$$J_{diff} = n \times F \times D \times \frac{c}{\delta}$$



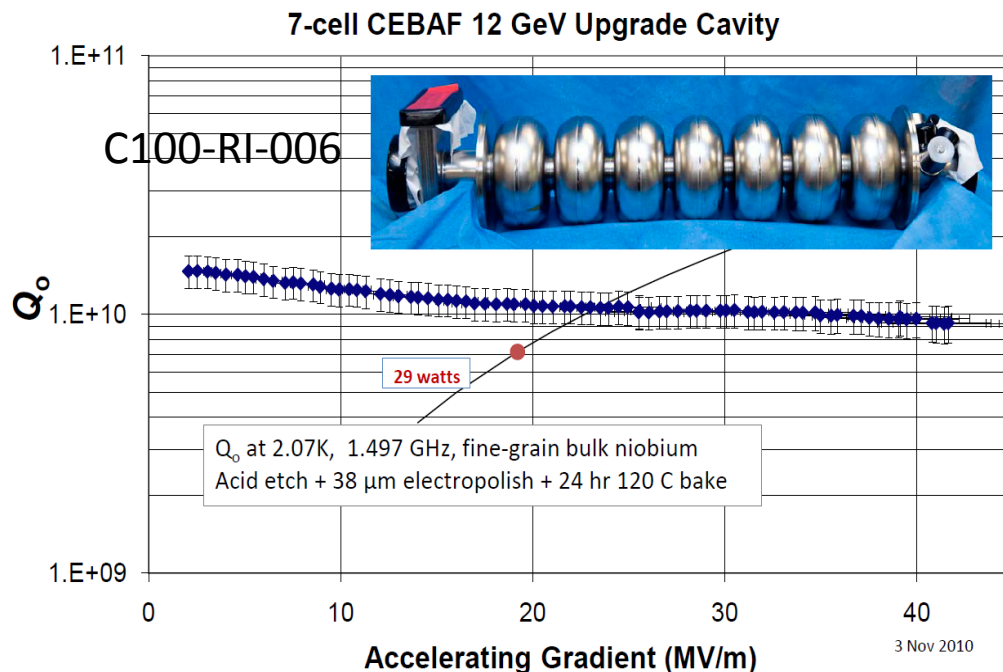
There exists a F ion concentration gradient within the ~12 μm (20°C) away the surface. Preferential dissolution of protrusions on the order of diffusion layer causes **enhanced geometrical leveling**. On this scale, initial material removal rate will not be blind to crystallography- **no brightening**.

Implications of basic understanding of EP

Positive Results from Controlled Light EP After BCP

For a well controlled, high reproducibility, efficient, reliable EP process.

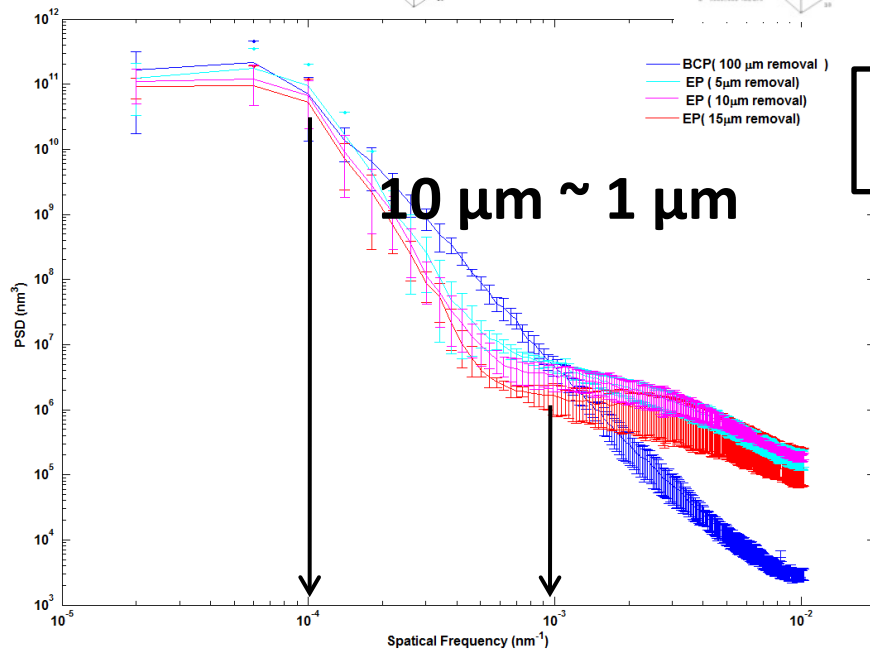
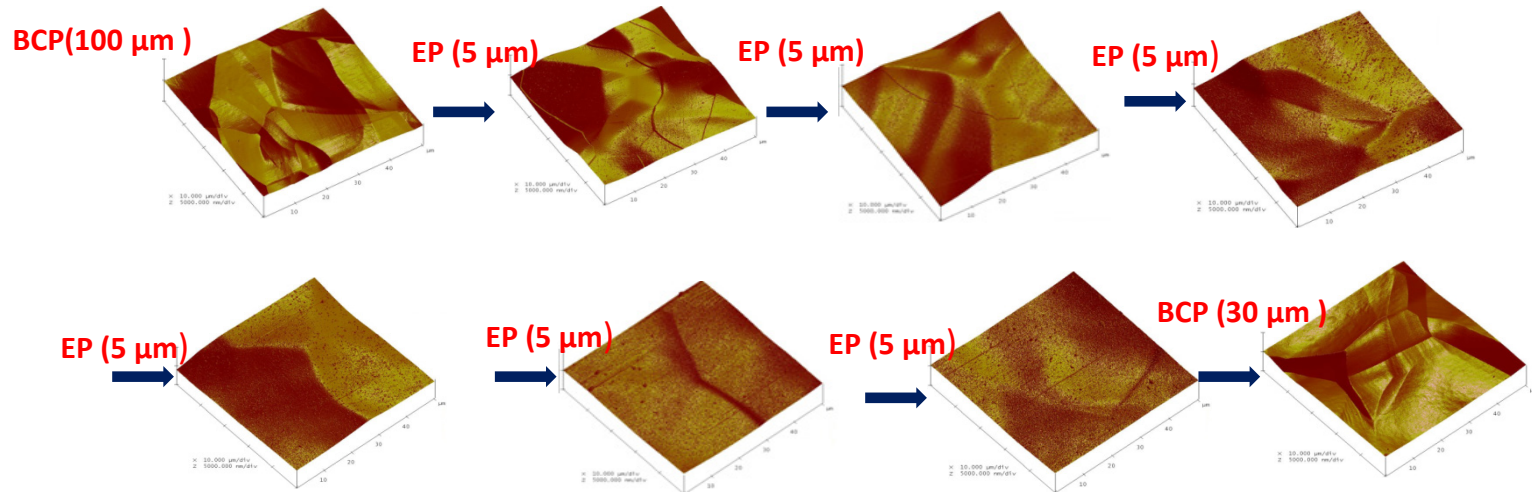
- ✓ Control and “minimize” the temperature as much as is practical.
- ✓ Minimize cathode current density, and over-potential (increase cathode surface area, improve reaction kinetics for hydrolysis).
- ✓ Start with surfaces that are consistently smooth below the scale of diffusion layer thickness, such as CBP (if objective is maximally smooth surfaces with minimum chemistry).
- ✓ Manage hydrogen bubbles and other forced or natural convection for maintaining a controlled local surface flow dynamics .



12 GeV Upgrade Project adopts it as an alternated baseline for the 80 cavities, the on-going production progresses steadily.

*“Preparation and Testing of the SRF Cavities for the CEBAF 12 GeV Upgrade”, **TUPO 061**, A. Reilly, T. Bass, A. Burrill, K. Davis, F. Marhauser, C.E. Reece and M. Stirbet.*

Scale-Specific Nb Surface Topographic Evolution During EP

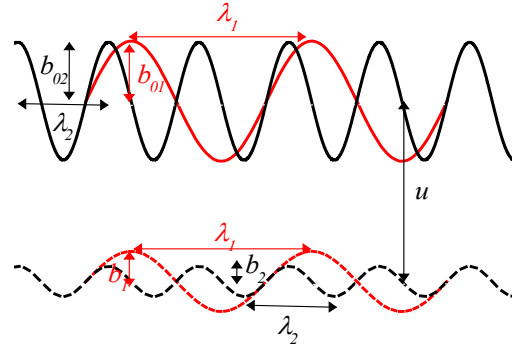
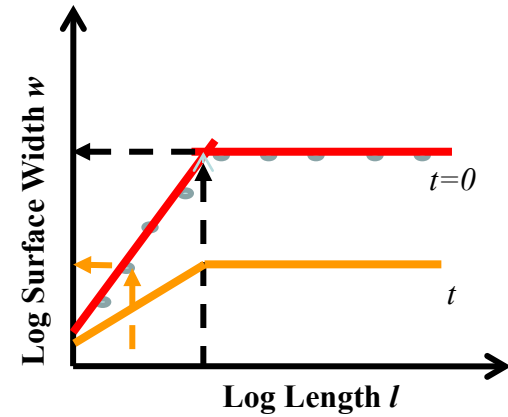


EP is conducted at 14 volts, 20 C with 15 mA/cm² same condition as Jlab 12 GeV cavity production.

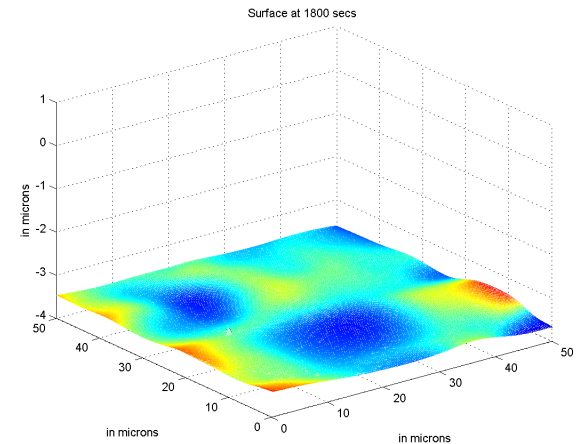
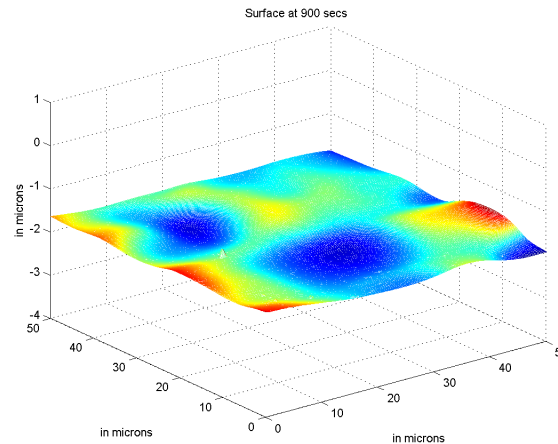
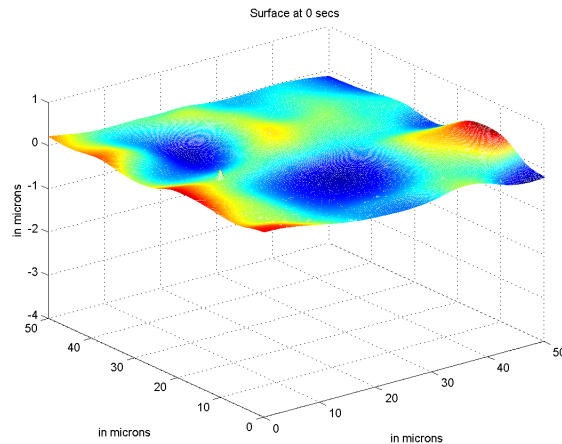
Short duration EP modifies the surface feature with wavelength from 1 μm ~ 10 μm -which might be important for SRF performance improvement.

"Characterization of scale-dependent roughness of niobium surfaces as a function of surface treatment processes detailed information", THPO046, C. Xu, H. Tian, C. Reece & M. Kelley .

Simulations of the Nb Surface Morphology Evolution During Electropolishing



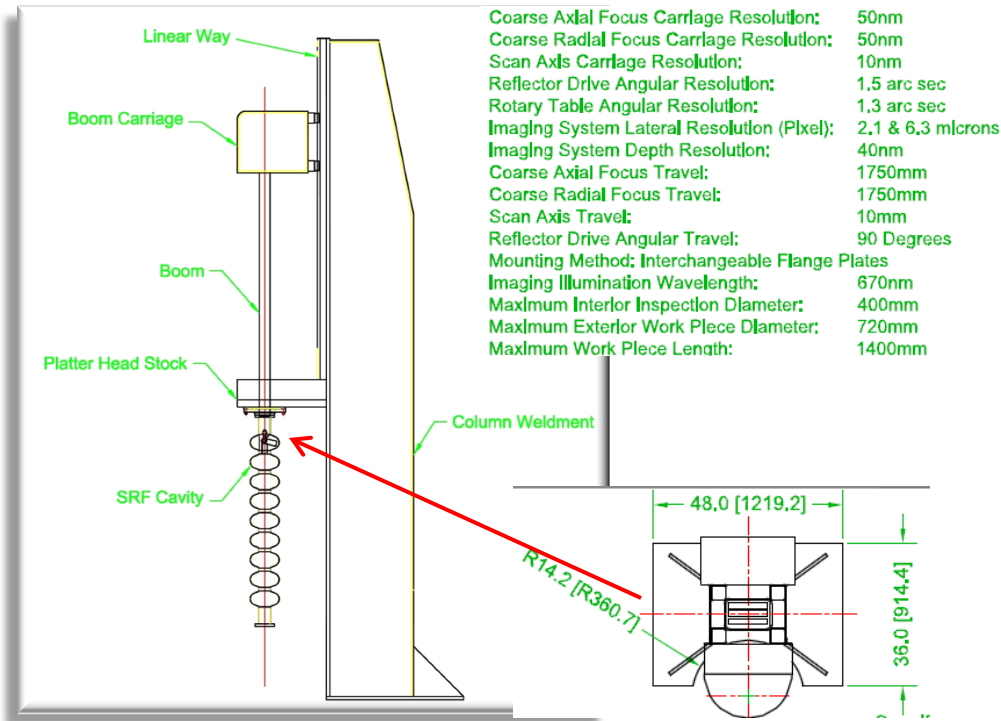
The morphology evolution of Nb surface during the electropolishing is described using a combined approach of scaling analysis and predictions of the electropolishing theory. Establishing the parameters of Nb EP process and the resulting surface smoothing.



Characterize the topographic transformation function sufficient to gain predictive power over topography as a function of EP time.

"Detailed Nb Surface Morphology Evolution During Electropolishing for SRF Cavity Production" THPO038, H. Tian, C. Reece, Nikhil Dole and Stanko Brankovic.

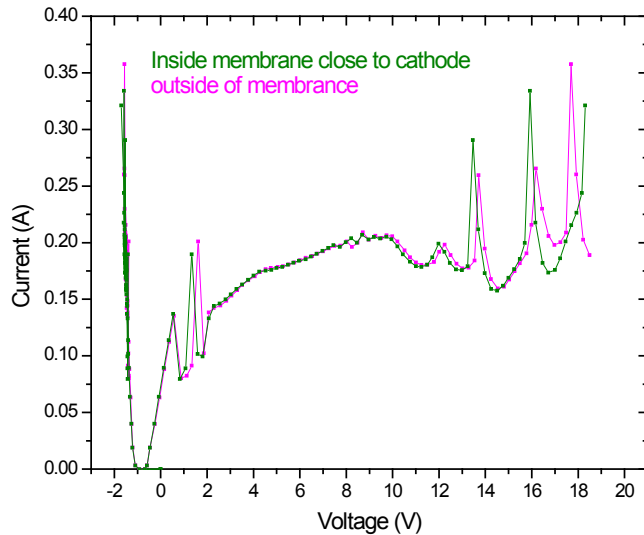
Closing the Loop from Sample Analysis to Single/Multicell Cavities with Internal Cavity Profilometry



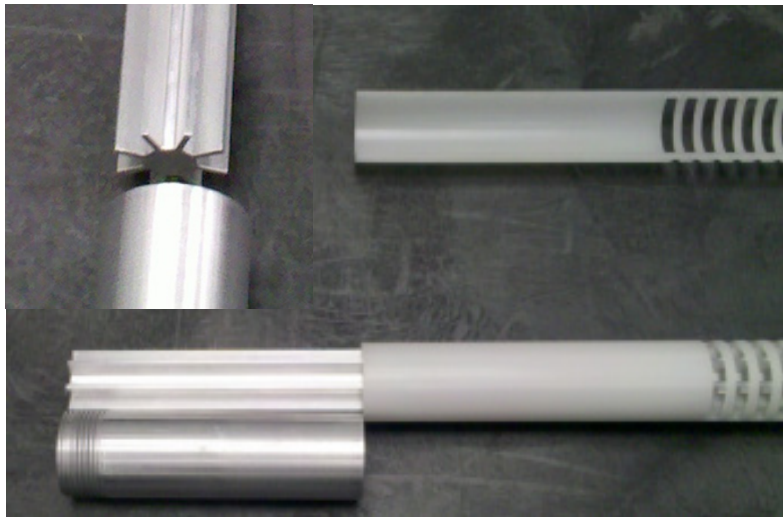
Microdynamics internal optical inspection system will be commissioned in this August. Enable detailed analysis of surface evolution as a function of EP parameters applied to single /multi-cell cavities.

Track specific features/limiting defects through processing, serves as a qualitative and quantitative defect inspection and 3-D surface mapping tool.

Incorporating Lessons Learned into Development of an Integrated Cavity Processing (ICP) System



- ✓ Hydrophobic PTFE membrane proves efficiently blocking hydrogen bubbles created at cathode, and maintains electropolishing process.
- ✓ Spline shape cathode increases cathode area, the introduction of circulation inside of membrane protected cathode drives out hydrogen bubbles without agitation near cavity surface.
- ✓ Commissioning a new, unused cavity chemical processing tool for present VEP studies, and planning to integrate HPR, ultrasonic detergent cleaning, and protected drying in this system in the near future (ICP) -reduce costs and assure appropriate process control - future ILC-like applications
- ✓ New Jlab infrastructure will be ready for such a tool next year



Our strategy (first step):

1. CBP for consistent, reproducible surface finish and removal of "damage" layer.
2. Minimal (10~20 μ m) , controlled, low-touch labor EP to expose clean, smooth, crystalline surface.

References:

- 1) A. J. Bard and L. R. Faulkner, *Electrochemical Methods*, Wiley: New York, 1980.
- 2) H. Tian, S. G. Corcoran, C. E. Reece and M. J. Kelley, *J. Electrochem. Soc.* 155(2008), p. D563.
- 3) V. Palmieri, *Proc. of 11th SRF workshop*, Travemünde/Lübeck, Germany (2003).
- 4) V.G. Levich, *Physicochemical Hydrodynamics*, Prentice-Hall, New York, 1962.
- 5) F. Eozénou, S. Berry, C. Antoine, Y. Gasser, J.-P. Charrier and B. Malk., *PhysRev-STAB* 13, 083501 (2010).
- 6) H. Tian and C. E. Reece, *PhysRev-STAB* 13, 083502 (2010).
- 7) C. Reece and H. Tian, *Proceeding of LINAC2010*, Tsukuba, Japan THP010.
- 8) H. Tian, C. Xu, C. E. Reece, and M. J. Kelley, *Appli. Surf. Sci* volume 257(11), pp. 4781 (2011).
- 9) C. Wagner, *J. Electrochem. Soc.*, 101, p.225 (1954).
- 10) F. Family, T. Vicsek, *J. Phys. A* 18, L75 (1985).

Thanks to:

Charlie Reece, Tony Reilly , Jim Follkie , Larry Philips, O. Trofimova,
Ari Palczewski, Peter Kneisel
M. Kelley (W&M), S. Brankovic (U. Houston)

THANK YOU